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SOOT OXIDATION KINETICS

FINAL REPORT

W. FELDER

U.S. ARMY RESEARCH OFFICE

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AEROCHEM RESEARCH LABORATORIES, INC. P.O. BOX 12 PRINCETON, NJ 08542



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## 20. ABSTRACT (Continue on reverse alds if necessary and identify by block number)

Soot and carbon black oxidation kinetics have been measured under controlled temperature, pressure, and oxygen concentration,  $[0_2]$ , tonditions in a modified High Temperature Fast Flow Reactor over the range 1000-1700 K and  $0.05 \le [0_2] \le 200 \times 10^{16}$  cm<sup>-3</sup>. The kinetic measurements are carried out under conditions where the carbon particle consumption rate is controlled by gas particle interactions and not by mass transfer. Auxiliary surface area measurements on partially oxidized particles collected from the HTFFR indicate that the oxidation is controlled by external surface rather than

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pore-centered reactions. The measured particle reactivities (g cm $^{-2}$  s $^{-1}$ ) are  $\times$  10 smaller than predicted by the often used Nagle-Strickland-Constable semiempirical model for carbon oxidation nor do the [0<sub>2</sub>] dependences conform to this model. Additional work is required to elucidate the reasons for this disparity.

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#### STATEMENT OF THE PROBLEM STUDIED

The objective of this research program was to measure oxidation rate constants (reactivities) for soot and soot-like carbon particles at temperatures between 1000 and 2000 K. Such measurements have been carried out over the temperature range 1000-1700 K for the  $0_2$  oxidation of three carbon blacks (soot-like materials) and soots collected from an ethylene/air diffusion flame. A modified AeroChem High Temperature Fast Flow Reactor (HTFFR) was used for most of the reactivity measurements. Additional preliminary measurements were made of the oxidation of soot in static, bulk sample experiments at temperatures as low as 740 K.

#### SUMMARY OF IMPORTANT RESULTS

The most important result of the HTFFR measurements is the finding that the measured reactivities do not conform to the widely accepted Nagle and Strickland-Constable (NSC) expression¹ developed from the two-site oxidation mechanism of Eyring and coworkers.² Neither the magnitudes nor the  $[0_2]$  dependences of the measured reactivities follow the predictions of the NSC formulation. It was speculated that the presence of large amounts of sulfur impurity in the carbon blacks studied might have been the cause of this anomalous behavior, but studies with "sulfur-free" soots did not support this conjecture while still showing disagreement with NSC predictions. It may be that the lower temperature range covered in these HTFFR studies than those generally used in the prior shock tube and flame studies of carbon particle oxidation (e.g., Refs. 3-6) is connected with this disagreement, but further work is needed to explore both this possibility and the effects of sulfur on the observed reactivities.

The physical and chemical properties of the carbon particles studied in this work are presented in Table I and illustrate the wide range of particle compositions and sizes studied. The carbon blacks were obtained commercially; two soots from the  $C_2H_4/air$  flame were used, one of which was "clean" while the other was contaminated with  $\approx 0.5$  wt.% Zn (the form of the Zn in the particles was not determined). The measured reactivities,  $R_e$  (g cm<sup>-2</sup> s<sup>-1</sup>), are presented in Table II along with their  $[O_2]$  dependences. In each case, an extremely wide range of  $[O_2]$  was covered to determine the order of the reaction in  $[O_2]$ , and in each case, only a single fractional order was found, rather than the change from first to zero order in  $[O_2]$  predicted from the two-site mechanism. No major effect of the Zn contamination of the  $C_2H_4/air$  soot was found on the oxidation rate.

In Table III and Fig. 1, the temperature dependences of the reactivities are illustrated for oxidation in "air" (20%  $O_2$ , 80%  $N_2$ ) at 101 kPa (1 atm). Under this condition, both the soot and carbon black oxidations exhibit similar activation energies of 120-140 kJ mol<sup>-1</sup>, consistent with previous measure-

ments (see, e.g., Ref. 7). Calculations indicate that for the range of particle sizes utilized in this work, mass transport (diffusion) of  $0_2$  to the particle surface is rapid compared to the observed reaction rates. Thus, the observed reactivities are controlled by the gas-particle reaction rate. Separate surface area measurements (by N2 gas adsorption with BET analysis) of partially oxidized particles collected from the HTFFR showed that the oxidation kinetics are well described by the simple "shrinking sphere" model in which a fully dense carbon particle undergoes external surface oxidation with concomitant decrease in radius. This is taken to indicate that particle porosity effects on the observed reactivities are negligible. Oxidation rate determinations (measured by weight loss per unit time) on bulk soot samples at 740 K in air (101 kPa) were made as a function of percentage of previous oxidation. The results show a small (< 25%) increase in the rate of oxidation as the fractional oxidation of the particles increases from 0 to 85%, perhaps indicating an increase in active surface area® with oxidation. The bulk oxidation reactivities at 740 and 950 K shown in Table II should be considered as preliminary values.

The main kinetic measurements were carried out in a uniquely modified AeroChem High Temperature Fast Flow Reactor (HTFFR). Part of the modifications involved development of a particle feed system for delivering stable flows of particle-laden diluent gas to the heated reactor in which these flows were mixed with  $O_2$  and additional diluent. The reaction time was controllable from 30-800 ms and oxygen concentrations between \* 1 × 10<sup>15</sup> and 2 × 10<sup>18</sup> cm<sup>-3</sup> were used. The extent of reaction was measured by gas chromatography (gc) by determining the amount of  $CO + CO_2$  produced for a given reaction condition. Carbon mass flow was also determined by gc by completely oxidizing the particles flowing into the HTFFR and measuring the  $CO + CO_2$  produced. The apparatus, technique, and results of carbon black oxidation studies are fully described in the publication listed below.

## **PUBLICATION**

"Oxidation Kinetics of Carbon Blacks over 1300-1700 K," W. Felder, S. Madronich, and D.B. Olson, submitted to Energy & Fuels.

## **PRESENTATIONS**

"Soot Oxidation Kinetics," W. Felder, presented at 7th ARO/Engine Fuels Work-shop, Wayne State University, 13-14 October 1987.

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"Oxidation Kinetics of Carbon Blacks over 1300-1700 K," W. Felder, and S. Madronich, presented at Fuel Division Symposium, Fall ACS Meeting, New Orleans, LA, 30 August-4 September 1987.

"Soot Oxidation Kinetics," W. Felder, D.B. Olson, and S. Madronich presented at 6th ARO/Engine Fuels Workshop, Davis, CA,17-18 March 1986.

"Soot Oxidation Kinetics," W. Felder, S. Madronich, and D.B. Olson, presented at Fall Technical Meeting, Eastern Section: The Combustion Institute, Philadelphia, PA, 4-6 November 1985.

"Soot Oxidation Kinetics," W. Felder, D.B. Olson, and S. Madronich presented at 5th ARO/Engine Fuels Workshop, Philadelphia, PA, 27-28 March 1984.

#### PERSONNEL

AeroChem personnel who contributed to this project were W. Felder, S. Madronich, D.B. Olson, R.J. Gill, D.G. Keil, H.F. Calcote, and L. Aldridge. No degrees were awarded.

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TABLE I

PHYSICAL AND CHEMICAL PROPERTIES OF CARBON PARTICLES

Carbon <u>Particle</u>	Mean Particle <u>Diam (nm)</u>	BET (N <sub>2</sub> ) Surface <u>Area (m²/q)</u>	Volatiles (wt. %)	Metal Content <sup>c</sup> (wt. %)	Ash (wt. %)	Sulfur
Raven 16ª (R16), Carbon Black	61	25 (294)	0.9	0.1	0.27	1.67
Conductex SC* (CSC), Carbon Black	20	220 (190)	1.5	0.08	0.49	0.85
Raven 850ª (R850), Carbon Black	31	70 (72%)		0.04	0.28	1.31
Soot (C <sub>2</sub> H <sub>4</sub> /Air)		1055	5.8	0.016	0.045	< 0.02▶
Soot (C <sub>2</sub> H <sub>4</sub> /Air + Zn)		1085	5.76	0.66	0.146	< 0.02₺

Data supplied by manufacturer, Columbian Chemical Co.

<sup>&</sup>lt;sup>c</sup> The measured metallic impurities contents (wt.%) are summarized below:

Metallic Impurity	R16*	_CSC*	_R850*	Soot b	Soot + Znb
Σ Mn, Mg, Al, Ti	0.007	0.008	0.002	0.007	0.030
Fe	0.045	0.005	0.003	0.005	0.051
Na	0.021	0.047	0.029	< 10-5	0.032
Ca	0.025	0.016	0.006	< 10-3	< 10-3
Zn	< 10-●	< 10-8	< 10-8	< 10-5	0.5

Properties measured in this work.

		log <sub>10</sub> R <sub>0</sub>		
Carbon		g cm <sup>-2</sup> s <sup>-1</sup>		[0 <sub>2</sub> ] range
<u>Particle</u>	T (K)	[O <sub>2</sub> ]-n)	n	(1016 cm-3)
Raven 16	1300	-16.3 ± 0.6b	0.62 ± 0.04b	0.2 - 158
(Carbon Black)	1400	$-16.5 \pm 2.0$	$0.64 \pm 0.12$	2.0 - 104
	1470	$-16.1 \pm 1.3$	0.66 ± 0.10	0.05 - 98
	1580	$-14.9 \pm 1.7$	$0.59 \pm 0.10$	0.12 - 177
	1680	$-15.1 \pm 1.0$	0.61 ± 0.07	0.18 - 154
Conductex SC	1410	$-18.6 \pm 0.5$	0.76 ± 0.13	0.04 - 200
(Carbon Black)	1580	-18.8 ± 1.1	$0.82 \pm 0.17$	0.2 - 132
	1650	$-14.2 \pm 1.4$	0.57 ± 0.08	0.3 - 75
Raven 850	1550	$-15.3 \pm 2.1$	0.62 ± 0.20	0.08 - 52
(Carbon Black)	1400	-16.6 ± 1.7	0.65 ± 0.15	0.9 - 61
	1300	$-16.0 \pm 1.5$	0.60 ± 0.15	1.0 - 95
Soot c	1400	$-16.1 \pm 1.1$	0.66 ± 0.05	0.1 - 120
(C <sub>2</sub> H <sub>4</sub> /Air)	1200	$-20.2 \pm 1.0$	$0.85 \pm 0.10$	0.1 - 170
	1000	-21.6 ± 2.2	0.85 ± 0.25	0.5 - 180
Soot' (0.5%	1400	-16.3 ± 1.2	$0.65 \pm 0.11$	0.1 - 100
wt. Zn)	1200	$-10.5 \pm 2.2$	0.80 ± 0.22	0.5 - 87
(C <sub>2</sub> H <sub>4</sub> /air)	1000	$-21.9 \pm 1.5$	0.88 ± 0.30	1.0 - 50
		10910 Re		
Sootc	950	- 8.6 ± 1.0	d	155
(C <sub>2</sub> H <sub>4</sub> /air)	740	$-10.5 \pm 1.0$	d	200

 $<sup>^{\</sup>mathrm{a}}$  g cm $^{\mathrm{-2}}$  s $^{\mathrm{-1}}$ ; gas concentration units, molecules cm $^{\mathrm{-3}}$ 

One standard deviation

Soot collected from ethylene/air diffusion flame.

<sup>•</sup> Measured at a single  $[0_2]$ .

TABLE III REACTIVITIES OF CARBON PARTICLES IN AIR (20%  $O_2$ , 80%  $N_2$ ) AT 101 kPa FROM HTFFR MEASUREMENTS Reactivity (g cm<sup>-2</sup> s<sup>-1</sup>)

Carbon Blacks				Sootsa		
T (K)	Raven 16	Conductex SC	Raven 850	C <sub>2</sub> H <sub>4</sub> /Air	$C_2H_4/air + 0.5%$ Z	
1680	6.9 × 10 <sup>-5</sup>					
1650		1.1 × 10-4				
1580	5.5 × 10-5	7.9 × 10-5				
1550			7.1 × 10-5			
1470	6.0 × 10-5					
1400	1.1 × 10-5	1.2 × 10-5	1.2 × 10-5	6.3 × 10-5	2.6 × 10-5	
1300	7.8 × 10-6		6.9 × 10-6			
1200				1.6 × 10-5	1.0 × 10-5	
1000				6.3 × 10-7	1.2 × 10-6	

Soot collected from ethylene/air diffusion flame.

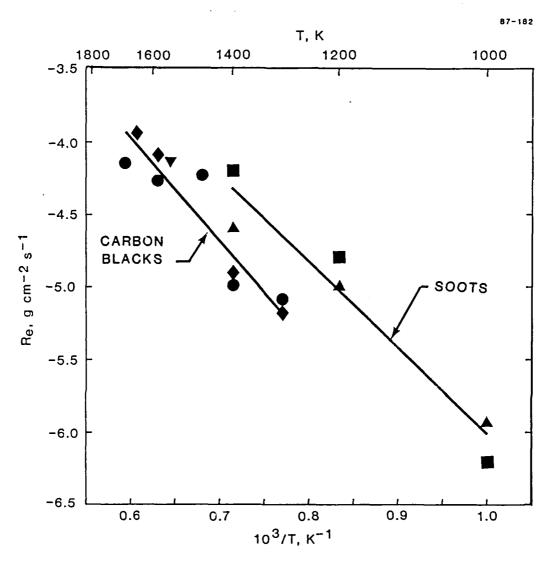


FIGURE 1 REACTIVITIES OF CARBON PARTICLES ABOVE 1000 K IN AIR (20%  $\rm O_2$ , 80%  $\rm N_2$ ) AT 101 kPa (1 atm)

- Carbon Black, Raven 16; ◆ Carbon Black, Conductex SC;
- ▼ Carbon Black, Raven 850; Soot, Ethylene/Air Flame;
  - ▲ Soot + 0.5% (wt.) Zn, Ethylene/Air Flame

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